Amendments to the Claims:

This listing of claims will replace all prior versions and listings of claims in the application:

Listing of Claims:

Claims 1-24 (cancelled)

25. (currently amended) A microcrystalline paraffin, prepared by hydroisomerizing, at temperatures above 200°C, FT (Fischer-Tropsch) paraffins having a carbon chain length distribution in the range from 20 to 105, attemperatures above 200°C, by processing the FT paraffins with a catalyst based on a beta zeolite, the catalyst comprising 60 to 95½ by mass of zeolite of the beta type, based on the combination of all components fired at 800°C, 5 to 39.8½ by mass of gamma-aluminum oxide having a specific surface area of 150-350 m²/g, calculated as Al_2O_3 and based on the combination of all components fired at 800°C, and one or more metals of transition group 8 of the periodic table, in an amount of 0.2 to 2.0% by mass, based on the combination of all components fired at 800°C, the one or more transition group 8 metals being attached to the gamma-aluminum oxide.

26. (previously presented) The microcrystalline paraffin according to claim 25, wherein, at 25° C the paraffin is not liquid but at least paste-like to solid with a needle penetration value of less than 100×10^{-1} mm, measured in accordance with DIN 51579.

- 27. (previously presented) The microcrystalline paraffin according to claim 25, wherein the paraffin is free of aromatic and heterocyclic compounds.
- 28. (previously presented) The microcrystalline paraffin according to claim 25, wherein the paraffin is free of naphthenes.
- 29. (previously presented) The microcrystalline paraffin according to claim 25, having a proportion by weight of isoalkanes that is greater than that of n-alkanes in the paraffin.

30. (cancelled)

31. (currently amended) Process for preparing a microcrystalline paraffin by catalytic hydroisomerization comprising

processing FT (Fischer-Tropsch) paraffins, as a starting material, having carbon atoms in the range from 20 to 105;

in the presence of a catalyst based on a ß-zeolite;

wherein the process is conducted at a temperature above 200°C, and

at a pressure in a range of 2 to 20 MPa in the presence of hydrogen;

wherein the catalyst comprises 60 to 95% by mass of zeolite of the beta type, based on the combination of all components fired at 800°C, 5 to 39.8% by mass of gamma-aluminum oxide having a specific surface area of 150-350 $\rm m^2/g$, calculated as $\rm Al_2O_3$ and based on the combination of all components fired at 800°C, and one or more metals of transition group 8 of the periodic table, in an amount of [[0.2]] $\rm 0.1$ to 2.0% by mass, based on the combination of all components fired at 800°C, the one or more transition group 8 metals being attached to the gamma-aluminum oxide.

- 32. (previously presented) Process according to claim 31, wherein the β -zeolite further comprises pores comprising a pore size between 0.50 and 0.80 nm.
- 33. (cancelled)
- 34. (cancelled)
- 35. (cancelled)
- 36. (previously presented) Process according to claim 31, wherein the pressure is 3 to 8 Mpa.
- 37. (previously presented) Process according to claim 31, wherein the process is conducted at a temperature of 230 to 270°C.

- 38. (previously presented) Process according to claim 31, wherein the hydrogen is fed to the paraffin, in a feed ratio of hydrogen to FT paraffin from 100:1 to 2000:1 standard m³ per m³.
- 39. (previously presented) Process according to claim 31, wherein the hydrogen is fed to the paraffin, in a feed ratio of hydrogen to FT paraffin from 250:1 to 600:1 standard m³ per m³.
- 40. (previously presented) Process according claim 31, wherein the process is carried out at a loading from 0.1 to 2.0 v/vh.
- 41. (previously presented) Process according to claim 32, wherein the catalyst has a pore size between 0.55 to 0.76 nm.
- 42. (cancelled)
- 43. (previously presented) Process according to claim 31, wherein the one or more metals of transition group 8 of the Periodic Table comprises platinum.
- 44. (currently amended) Process according to claim 43, wherein the platinum content of the catalyst is [[0.1]] 0.2 to 2.0% by mass, based on a catalyst fired at 800°C.
- 45. (previously presented) Process according to claim 31, wherein the FT paraffins have a solidification point ranging from 70 to 105°C.
- 46. (previously presented) Process according to claim 31, wherein the microcrystalline paraffin is prepared from the FT paraffins in a single process step.

Claims 47-50 (cancelled)

51. (previously presented) Process according claim 31, wherein the process is carried out at a loading from 0.2 to 0.8 v/vh.

- 52. (previously presented) Process according to claim 43, wherein the platinum content of the catalyst is 0.4 to 1.0% by mass, based on a catalyst fired at 800°C.
- 53. (previously presented) Process according to claim 45, wherein the FT paraffins have solidification points of 70, 80, 95 or 105°C.
- 54. (previously presented) Process according to claim 46, wherein the microcrystalline paraffins are prepared from the FT paraffins in a single process step, with removal of the short chain constituents.